



## EFFECT OF THE OUTLET NOZZLE DIAMETER ON THE PERFORMANCE OF DIVERGENT VORTEX TUBE

Dr. Asaad T. Al-Omran  
Technical College  
Baghdad

Dr. Ramzi R. Ibrahim  
Ins. Of Technology  
Baghdad

Dr. H. N. Al-Rawi  
Unv. Mamoon College  
Baghdad

### ABSTRACT

The aim of the present work is to study the effect of different outlet nozzle diameters, by using one or two nozzles on the performance of divergent vortex tube and also to determine the effects of various parameters on the vortex tube cooling performance such as: refrigeration capacity, coefficient of performance, isentropic efficiency. The experimental investigation was carried out on a divergent vortex tube rig manufactured for the present study covering all tests. The effect of different outlet nozzle diameters ( $d_n=4$  mm,  $d_n=5$  mm, and  $d_n=6.5$  mm) on the performance of the vortex tube is described by using one nozzle or two nozzles by varying the pressure of the inlet air and cold air mass ratio ( $\mu_c$ ) within the ranges ( $P_{i\ abs}=2 - 7$  bar) and ( $\mu_c=0 - 1$ ). The outlet nozzle diameter, ( $d_n=5$  mm), and the outlet cold diameter ( $d_c=10$  mm), when using two nozzles, give high temperature separation and may considered to be the optimum for different pressures of the inlet air regarding all the size tube diameter. The experimental study predicts two empirical results between the outlet nozzle diameter ( $d_n$ ), number of nozzles ( $N$ ), inside vortex tube diameter ( $D$ ), and length of vortex tube ( $L$ ) as:

$$\frac{Nd_n^2}{D^2} = 0.105 \quad \text{for } (N=1) \text{ and};$$

$$\frac{Nd_n^2}{D^2} = 0.211 \quad \text{for } (N=2)$$

### الخلاصة

الهدف من البحث الحالي هو دراسة تأثير القطر الداخلي للمناث باستخدام منفت واحد ، ومنفتان على أداء الأنبوب الدوامي المنفرج ، وكذلك دراسة مختلف العوامل التي تؤثر على الأداء التبريدي مثل سعة التبريد ، معامل الأداء ، الكفاءة الايزنتروبية. أنجزت التجارب من خلال بناء جهاز متكامل للأنابيب الدوامية المنفرجة ، صمم

وصنع خصيصاً لهذا البحث، حيث غطى جميع التجارب. تمت دراسة تأثير تغير القطر الداخلي للمنفث (  $d_n = 4 \text{ mm}, 5 \text{ mm}, 6.5 \text{ mm}$  ) وذلك باستخدام منفث واحد ، ومنفتان ، على أداء الأنبوب الدوامي المنفرج ، مع تغير الضغط المطلق للهواء الداخل ونسبة كتل الهواء البارد الى الهواء الداخل (  $\mu_c$  ) ضمن المدايات ( 2-7 bar ) و (  $\mu = 0 - 1$  ) على التوالي. عند استخدام فتحة المنفث (  $d_n = 5 \text{ mm}$  ) وفتحة البارد الخارج (  $d_c = 10 \text{ mm}$  ) وباستخدام منفثان تعطي اعلى فصل في درجة الحرارة ويمكن اعتبارها الامثل لضغوط المختلفة الداخلة الى الانبوب الدوامي . تم الحصول على علاقتين تجريبية تربط قطر المنفتات ، عدد المنفتات ، القطر الداخل للأنبوب (D)، طول الأنبوب. ( L ) بحيث تعطي افضل تصميم للأنبوب الدوامي المنفرج ذو طاقة فصل عالية، كالتالي :

$$\frac{Nd_n^2}{D^2} = 0.105 \quad N=1$$

$$\frac{Nd_n^2}{D^2} = 0.211 \quad N=2$$

## KEY WORDS

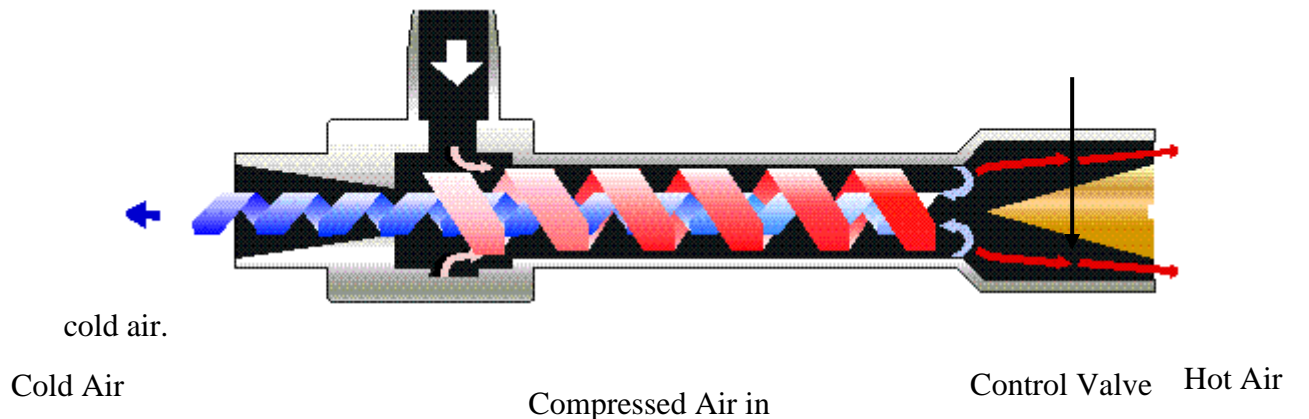
Counter Flow Vortex Tube , Thermal / temperature Separation , Design

### Parameters

## INTRODUCTION

A vortex tube uses compressed air as a power source, has no moving parts and produces hot air from one end and cold air from the other, as shown in **Fig.1**.

There is one widely accepted explanation of the phenomenon: (**Prasad 1963 , vortex tube theory 2000**). Compressed air is supplied to the vortex tube and passes through nozzles that are tangent to the internal counterbore. These nozzles set the air in a vortex motion. The spinning stream of air turns and passes down the hot tube in the-form of a spinning shell, similar to a tornado. A valve at one end of the tube allows some of the warmed air to escape. What does not escape, heads back down the tube as a second vortex inside the low-pressure area of the larger vortex. The inner vortex losses heat and exhausts through the other end as



**Fig.1:** Diagrammatic view of the pattern in a counter-flow tube .



While one air stream moves up the tube and the other down it, both rotate in the same direction at the same angular velocity. Due to the principle of conservation of angular momentum the speed of the inner vortex remains the same. Angular momentum has been lost from the inner vortex. The energy lost shows up as heat in the out vortex. Thus the outer vortex becomes warm, and the inner vortex is cooled.

A number of researches mention the effects of tapering the vortex tube, with conflicting results. ( **Martynovskii and Alekseev 1957**), find a contracting hot tube to be preferable and get optimum performance for  $(40 < L/D < 50)$  which is comparable to (**Hilsch's 1947**) comment that  $(L/D)$  should be around (50) for good temperature separation.

(**Raiskii and Tunkel 1974**) investigated the influence of the vortex tube configuration (cylinder, diffuser and step), on the vortex-temperature gas-separation process. Results show that long cylindrical tubes are most effective in a broad range of variations of structural and modal parameters, noting that the majority of the energy transfer appears to occur within the first five diameters of the tube.

(**Soni and Thomson 1975**) employed a systematic method of experimental design to determine the optimum performance of a vortex tube as a function of the pertinent design parameters, especially the individual experiments were stipulated according to the simplex modification of the method of evolutionary operations, (**EVOP 1962**).

The results indicate the following optimum design parameters for maximum  $(\Delta T_c)$  and maximum isentropic efficiency  $(\eta_{ise})$ .

$$A_N (\text{Nozzle / tube area}) = 0.11 \pm 0.01 (0.08 \pm 0.001)$$

$$A_\phi (\text{Orifice area / tube area}) = 0.08 + 0.01 (0.145 \pm 0.035)$$

(**Takahama and Yakosawa 1981**) investigated the measurements of the swirling flows inside the divergent chambers. The results show that the shorter divergent chambers ( $L=900$  mm) have a higher angular velocity near the center of the back flow and the swirl intensity increases in divergent chambers in the direction of flow with relatively large divergent angles.

(**Mitushen and Mohammed 1992**), part I, designed " Laser Doppler Velocimeter" that provides three velocity components of the flow inside the counter flow vortex tube. Results indicate a reverse flow from the axial velocity profiles in the central region ( $r < 4 - 5$ ) mm of the vortex tube and the maximum axial velocity was is to the tube wall.

(**AL-Abriy 1997**) carried out an experimental study on the effect of tangential nozzles number on the performance of vortex tube by varying the number of tangential nozzles to become between (1-8) nozzles under inlet pressure of (3-7) bar at cold air mass fractions of  $(\mu_c = 0-1)$ .

A laboratory device, "Hilton Co. Manufacture" and rig employed by (**Al-Jielawe 1994**) were used to carry out the experiments studying.

Results show that there is an optimum value of number of nozzles ( $N = 8$  and  $d_c = 0.8$  mm) to get high performance.

(**AL-Barwari 2004**) studied the experimental study on the thermodynamic properties of vortex tubes with a divergent chamber. The experimental investigation was carried on a divergent vortex tube rig especially designed for the present study covering all tests. The effect of different cold outlet diameters ( $d_c=10$  mm,  $d_c=12$  mm, and  $d_c=14$  mm ) on the performance of the vortex tube is described .The results show a pronounced influence of divergent vortex tube ( $\theta^\circ = 1.72$ ,  $L= 460$  mm), on the energy separation performance.

## REFRIGERATION PERFORMANCE

Performance of simple refrigeration plant is usually characterized by means of the Coefficient of Performance (C.O.P) defined for the cyclic work-absorbing device **Fig.2** as (**vortec corporation catalogue 1992**).

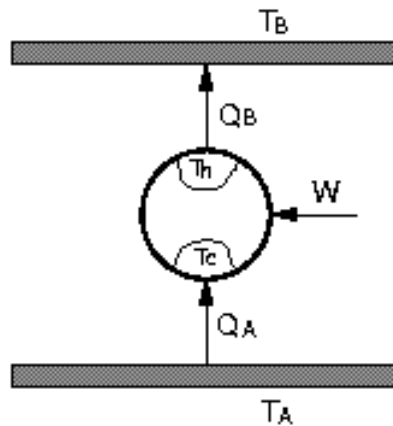


Fig (2) cyclic work absorbing device.

$$\text{COP} = \frac{Q_A}{W_{\text{act}}} \quad (1)$$

The process of ideal compression of the inlet air mass from the atmospheric pressure ( $P_a$ ) to high pressure ( $P_i$ ) is represented by the line ( $T_i - T_f$ ) in **Fig.3** and the actual compression is represented by the line ( $T_i - T_f'$ ). [13]

The COP of the vortex tube is defined as the ratio of the actual cooling effect to the work input to the air-compressor.

The compressed air has to be cooled at constant pressure in a cooler to the initial temperature ( $T_i$ ) before being sent to the vortex tube. The refrigeration capacity (actual cooling) of the vortex tube is simply equal to  $Q_r$ .

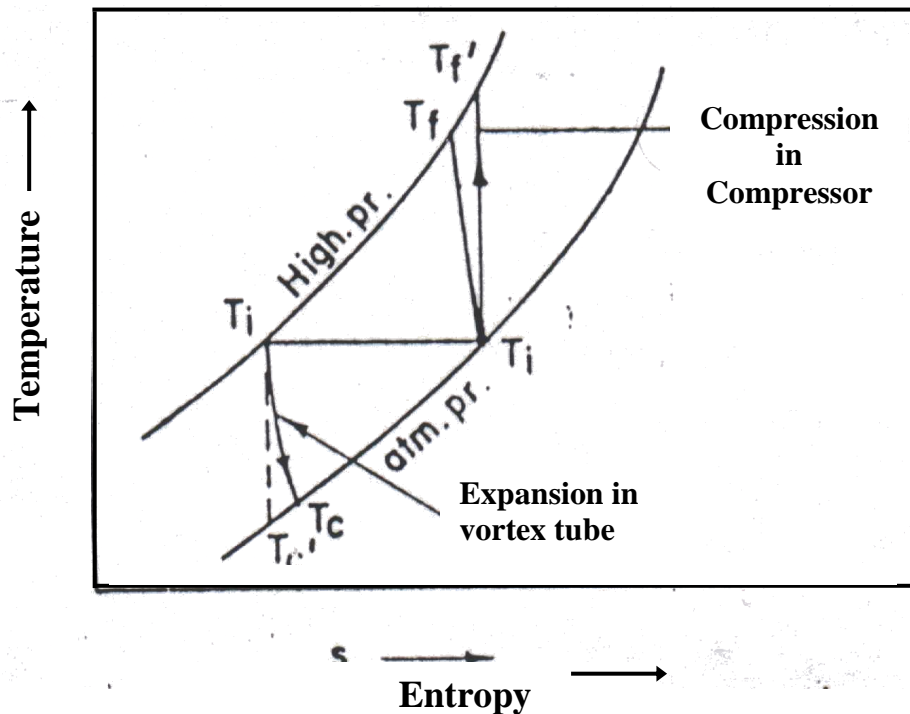


Fig.3:

Compression and expansion

process in a vortex tube

$$Q_r = m_c C_p (T_i - T_c) \quad (2)$$

Thus:

$$COP = \frac{m_c C_p \Delta T_c \eta_{comp}}{m_i C_p T_i \left[ \left( \frac{P_i}{P_a} \right)^{\frac{\gamma-1}{\gamma}} - 1 \right]} \quad (3)$$

If the process undergoes an isentropic expansion from the inlet pressure ( $P_i$ ) to atmospheric pressure ( $P_a$ ) at the cold end then the static temperature drop due to expansion is given by:

$$\Delta T_{c'} = T_i - T_{c'} = T_i \left[ 1 - \left( \frac{P_a}{P_i} \right)^{\frac{\gamma-1}{\gamma}} \right] \quad (4)$$

The actual temperature drop due to expansion occurred in vortex tube is  $\Delta T_c$  the ratio of  $\Delta T_c$  to  $\Delta T_{c'}$  is called “Relative Temperature Drop”.

$$R.T.D = \frac{\Delta T_c}{\Delta T_{c'}} \quad (5)$$

The adiabatic (isentropic) efficiency of the vortex tube is defined as:

$$\eta_{ise} = \frac{\text{Actual Cooling effect obtained in the vortex tube}}{\text{Ideal cooling effect possible with adiabatic expansion}}$$

$$\eta_{ise} = \mu_c \frac{\Delta T_c}{\Delta T_{c'}} \quad (6)$$

Sub. Eq. (4) in (6) one gets:

$$COP = \mu_c \left( \frac{\Delta T_c}{\Delta T_{c'}} \right) \eta_{comp} \left( \frac{P_a}{P_i} \right)^{\frac{\gamma-1}{\gamma}} \quad (7)$$

By substituting the value of  $\left( \mu_c \frac{\Delta T_c}{\Delta T_{c'}} \right)$  from Eq.(6), in Eq.(7), one gets:

$$COP = \eta_{ise} \eta_{comp} \left( \frac{P_a}{P_i} \right)^{\frac{\gamma-1}{\gamma}} \quad (8)$$

## EXPERIMENTAL APPARATUS AND RIG LAYOUT

The test rig is designed and manufactured to fulfill the requirements of the test system for different divergent vortex tube. The main rig, and the apparatus of the system illustrated in Figs. 4 and 5 and photograph (1).

## RESULTS AND DISCUSSION

Effect of cold air mass ratio ( $\mu_c$ ) on the temperature difference ( $\Delta T_h, \Delta T_c$ ), isentropic efficiency ( $\eta_{ise}$ ) coefficient of performance (COP), and refrigeration capacity (QR), for the inlet air pressure change and outlet nozzle diameter ( $d_n$ ), are investigated .

**Fig.6** at ( $P_{i abs} = 7$  bar), number of nozzle = 1, and, ( $\mu_c = 0.408$ ), shows, that the best energy separation, i.e highest temperature separation is for the outlet nozzle diameter ( $d_n=6.5$  mm), and ( $d_c = 10$  mm), in respect with all selected outlet nozzle diameters, which give the minimum values of the cold air temperature differences ( $\Delta T_c$ ), as shown in **Table (1)**

Table (1): Results of One Nozzle

Number of nozzles = 1, D= 20 mm, L/D = 23, L = 460, ( $\theta^\circ = 1.72$ ), $T_{in} = 30^\circ C$ $d_c=10$ mm					
$d_n = 4$ mm		$d_n = 5$ mm		$d_n = 6.5$ mm	
Minimum $T_c(^{\circ}C)$	Maximum $T_h(^{\circ}C)$	Minimum $T_c(^{\circ}C)$	Maximum $T_h(^{\circ}C)$	Minimum $T_c(^{\circ}C)$	Maximum $T_h(^{\circ}C)$
1.2	55.2	-14.5	71.2	-20	72.3

**Fig.7**, at ( $P_{i abs} = 7$  bar ), ( number of nozzles = 2 ), ( $\mu_c = 0.409$ ). shows clearly, that the best performance is for the outlet nozzle diameter ( $d_n = 5$  mm), and ( $d_c = 10$  mm), which gives the minimum values of the cold air temperature i.e maximum temperature differences ( $\Delta T_c$ ), and the maximum value of the hot temperature, i.e the highest value of the hot temperature, as shown in **Table (2)**:

Table (2): Results of Two Nozzle

Number of nozzles = 2, D = 20 mm, L/D = 23, L = 460, ( $\theta^\circ = 1.72$ ), $T_{in} = 30^\circ C$ $d_c = 10$ mm					
$d_n = 4$ mm		$d_n = 5$ mm		$d_n = 6.5$ mm	
Minimum $T_c(^{\circ}C)$	Maximum $T_h(^{\circ}C)$	Minimum $T_c(^{\circ}C)$	Maximum $T_h(^{\circ}C)$	Minimum $T_c(^{\circ}C)$	Maximum $T_h(^{\circ}C)$
-20.2	70.5	-35.5	81.2	-34.1	77.5

In **Figs. 8, 9** and **10** samples are selected to illustrate the effect of outlet nozzle diameter on isentropic efficiency with two nozzles at outlet cold diameter ( $d_c=10$  mm ) as illustrated in **Table (3)** for different outlet nozzles diameters.

Table (3): Isentropic Efficiency Results

One nozzle				Two nozzles			
$d_c = 10$ mm				$d_c = 10$ mm			
	$d_n = 4$ mm	$d_n = 5$ mm	$d_n = 6.5$ mm	$d_n = 4$ mm	$d_n = 5$ mm	$d_n = 6.5$ mm	$P_{i abs}$



$\eta_{ise}$	10.58	18.25	22	22.9	28.2	27.9	2
%							
$\mu_c$	0.601	0.718	0.706	0.714	0.703	0.714	7
$\eta_{ise}$	6.22	13.38	18.1	18.8	20.6	21.8	
%							7
$\mu_c$	0.607	0.617	0.707	0.715	0.702	0.713	

In Figs. 11, 12 and 13 samples are selected to show the effect of changing ( $\mu_c$ ) on (COP) of vortex tube ( $\theta^\circ = 1.72$ ), at ( $L/D = 23$ ) for different pressure ranges between (2-7) bar, with two nozzles at outlet cold diameter ( $d_c = 10$  mm).

The best values were acquired for the above mentioned outlet nozzle diameters, as illustrated in Table (4):

Table (4): Effect of Cold Air Ratio Optimum Results of COP

One nozzle				Two nozzles			
$d_c = 10$ mm				$d_c = 10$ mm			
	$d_n = 4$ mm	$d_n = 5$ mm	$d_n = 6.5$ mm	$d_n = 4$ mm	$d_n = 5$ mm	$d_n = 6.5$ mm	$P_{i abs}$
COP	0.05	0.094	0.126	0.127	0.180	0.159	2
$\mu_c$	0.701	0.616	0.606	0.714	0.712	0.604	
COP	0.035	0.079	0.09	0.094	0.125	0.108	7
$\mu_c$	0.702	0.612	0.605	0.712	0.711	0.603	

Figs. 14, 15 and 16, show the effect of changing ( $\mu_c$ ) on the refrigeration capacity for vortex tube ( $\theta^\circ = 1.72$ ) at ( $L/D = 23$ ) for the pressure range between ( $P_{i abs} = 2-7$ ) bar, with two nozzles at outlet cold diameter ( $d_c = 10$  mm).

The best values acquired for the above mentioned outlet nozzle diameters at highest pressure ( $P_{i abs} = 7$  bar) and minimum at pressure ( $P_{i abs} = 2$  bar), are shown in Table (5):

Table (5): Effect of Cold Air Ratio Optimum Results of Qr

One nozzle				Two nozzles			
$d_c = 10$ mm				$d_c = 10$ mm			
	$d_n = 4$ mm	$d_n = 5$ mm	$d_n = 6.5$ mm	$d_n = 4$ mm	$d_n = 5$ mm	$d_n = 6.5$ mm	$P_{i abs}$
Qr, watt	15.7	33.25	60.03	54.81	150.5	149.51	2
$\mu_c$	0.601	0.616	0.706	0.718	0.714	0.714	
Qr, watt	308	610	1180	1284	1875.8	1866	7
$\mu_c$	0.611	0.617	0.712	0.716	0.713	0.714	

## CONCLUSIONS

- The outlet nozzle diameter ( $d_n = 6.5$  mm), and the outlet cold diameter, ( $d_c = 10$ ), when using **one nozzle** give a high temperature separation and may considered to be the optimum for different pressures of the inlet air regarding the size of tube diameter.
- The outlet nozzle diameter, ( $d_n = 5$  mm), and the outlet cold diameter ( $d_c = 10$  mm), when using **two nozzles**, give high temperature separation and may considered to be the optimum for different pressures of the inlet air regarding all the size tube diameter.
- The isentropic efficiency of the divergent vortex tube ( $\theta^\circ = 1.72$ ), ( $L/D = 23$ ), ( $L = 460$  mm), ( $d_c = 10$  mm), ( $d_n = 6.5$  mm), when using one nozzle and two nozzles, increase with cold air mass ratio ( $\mu_c$ ) and reaches the highest value at ( $\mu_c = 0.6-0.72$ ). On the other hand they decrease with the inlet air pressure increase. Divergent vortex tube ( $\theta^\circ = 1.72$ ) has a highest isentropic efficiency attain: ( $\eta_{ise} = 27.9$  %) at ( $\mu_c = 0.714$ ), when using **two nozzles**.
- The coefficient of performance (COP) of the divergent vortex tube ( $\theta^\circ = 1.72$ ), ( $L/D = 23$ ), ( $L = 460$  mm), ( $d_c = 10$  mm), ( $d_n = 6.5$  mm), when using one nozzle and two nozzles, increase with cold air mass ratio ( $\mu_c$ ) and reaches the highest value at ( $\mu_c = 0.6-0.72$ ). On the other hand they decrease with the inlet air pressure increase. Divergent vortex tube ( $\theta^\circ = 1.72$ ) has a highest coefficient of performance attain: (COP = 0.159 %) at ( $\mu_c = 0.604$ ), when using **two nozzles**.
- The refrigeration capacity of the divergent vortex tube ( $\theta^\circ = 1.72$ ) when using one nozzle and two nozzles is increased with cold air mass ratio ( $\mu_c$ ) till reaching the highest value at ( $\mu_c = 0.6 - 0.72$ ). They increase with the inlet air pressure increase and has a higher refrigeration capacity attain: ( $Q_r = 1866$  Watt) at ( $\mu_c = 0.714$ ), when use **two nozzles**.

## REFERENCES

- AL-Abriy, Z. T. "Effect of tangential nozzles number on the Performance of the vortex tube". Master's Thesis, University of Technology, Mech. Eng. Dep. Baghdad, Iraq, December 1995.
- AL-Jielawe, A. F. "Effect of divergent angle on the Performance of Vortex tube". Master's Thesis, University of Technology, Mech. Eng. Dep. Baghdad, Iraq, September 1994.
- AL- Barwari, R. R. I., "Experimental Study on The Thermodynamic Properties of Vortex Tubes With a Divergent Chamber". Ph. D. thesis, University of Technology, Mech. Eng. Dep., Baghdad Iraq, February 2004.
- Hilsch, R. "The use of the expansion of gases in a centrifugal field as a cooling process". *The Review of Scientific Instruments*, vol.18, No. 2, pp. 108-113, Feb. 1947.
- Mitushen, A.I and Mohammed, A. K. Part I: "Design and construction of Laser Doppler Velocimeter", Part II: "Visualization of the spiral flow inside the vortex tube by using laser". *Soviet researches, The library Of gas and Oil Institute*, Vol. 10, and 11 Moscow, 1992.





Martynovskii, V. S., and Alekseev, V. P. "Investigation of the vortex thermal separation effect for gases and vapors." *Technical physics*, vol.26, No. 2, pp. 2233-2243, 1957.

Prasad, M. "*Refrigeration and Air-conditioning*." 5<sup>th</sup>. Ed., July, pp. 174-179, 1996.  
Raiskii, Y. D., and Tunkel, L. E. "Influence of vortex tube configuration and length on the process of energetic gas separation." *Journal of engineering physics*, vol.27, No. 6, pp. 1578-1581, December 1974.

Soni, Y. and Thompson, W. J. "Optimal design of the Ranque-Hilsch Vortex tube". Transaction of the ASME, *Journal of Heat Transfer*, pp. 316-317, May 1975.

Spendley, W., Hext, W., and Himsvarth, F. R. "Sequential application of simplex design in optimization and Evolutionary operation". *Technometrics*, vol.4, pp. 441-461, 1962.

Takahama, H. and Yokosawa, H. "Energy separation in vortex tubes with a divergent Chamber". *Transactions of the ASME, Journal of Heat Transfer*, vol.103, pp. 196-203, May 1981

Vortex tube theory. <http://www.free-serve.co.uk/rhvtmati/explan.htm>, 2000.  
*Vortec Corporation Catalogue. Company Catalogue*, 10125 Carver Road, Cincinnati, Ohio, USA, 1992. UK Distributor: MEECH VORTEC, Burford House, 15 Thorney, Leys Business Park, Witney, Oxford, OX87GE

## NOMENCLATURE

$A_c, A_h$	Cross sectional area of the cold end orifice and hot end of the outlet air	$\text{m}^2$
$A_i$	Cross sectional area of inlet pipe	$\text{m}^2$
COP	Coefficient of performance	-
$C_p$	Specific heat at constant pressure	J/kg. K
$D$	Inner diameter of vortex tube	mm
$d_c$	Diameter of cold end orifice	mm
$d_h$	Diameter of hot end outlet	mm
$d_n$	Diameter of nozzle outlet	mm
$h_i$	Specific enthalpy of the inlet air	J/kg
$L$	Length of vortex tube	mm
$L/D$	(Length / inner diameter) of the vortex tube	-
$\dot{m}$	Mass flow rate per nozzle	kg/s
$\dot{m}_i, \dot{m}_c, \dot{m}_h$	Mass flow of inlet air, cold air and hot air	kg/s
$P_a$	Ambient pressure	bar
$P_i, P_c, P_h$	Pressure of the inlet air, cold air and hot air	bar
$Q_r$	Refrigeration capacity	Watt
$Q$	Heat exchanged between the system and its surrounding	Watt
$T_a$	Ambient temperature	$^{\circ}\text{C}$
$T_i, T_c, T_h$	Temperature of the inlet air, cold air and hot air	$^{\circ}\text{C}$
$T_o$	Temperature at the nozzle outlet	$^{\circ}\text{C}$

$\Delta T_c$	Temperature difference of cold air = $T_c - T_i$	$^{\circ}\text{C}$
$\Delta T c'$	Isentropic (maximum) temperature difference	$^{\circ}\text{C}$
$\Delta T_h$	Temperature difference of the hot air = $T_h - T_i$	$^{\circ}\text{C}$
$\eta_{\text{comp}}$	The isentropic efficiency of the compressor	%
$\eta_{\text{ise}}$	Isentropic efficiency of the vortex tube	%
$\theta$	Angle of divergence	degree
$\mu_c$	Cold air mass ratio = $\frac{m_c}{m_i}$	-
$\rho$	Density of the air	$\text{kg/m}^3$
c, h, i	Subscripts refer to cold, hot and inlet air	-

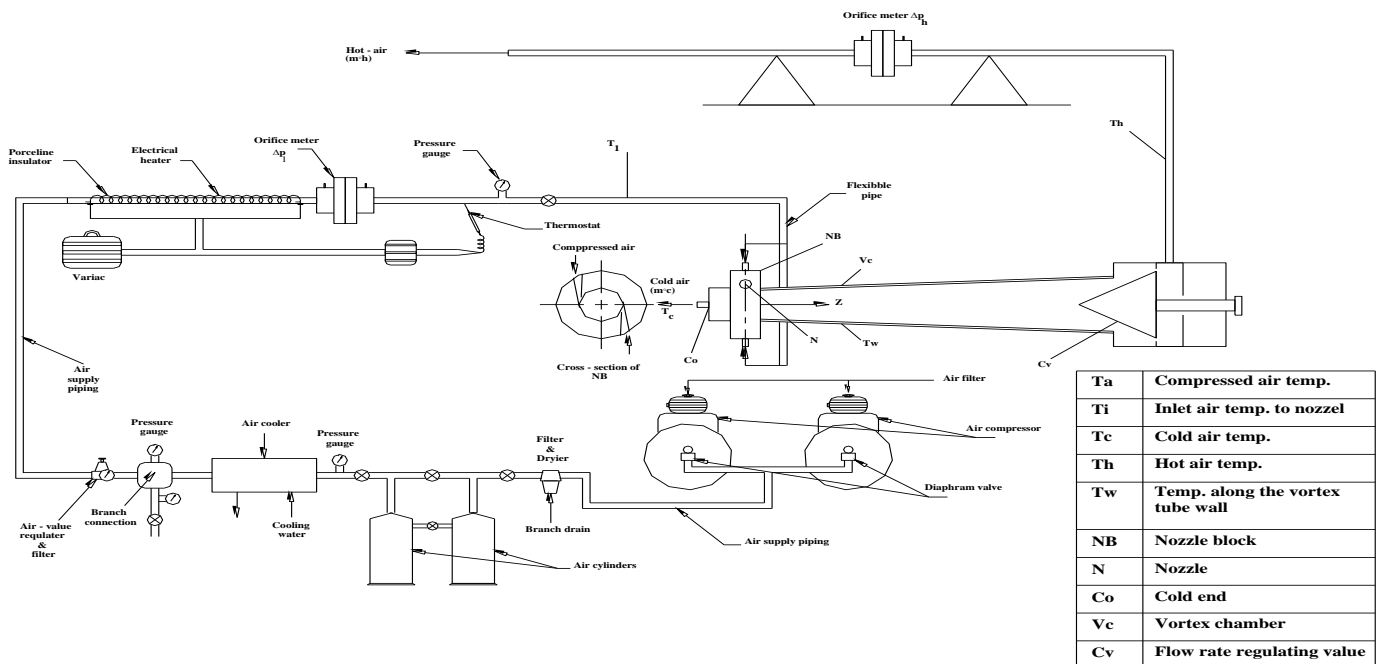


Fig. (4) Schematic diagram of the experimental rig.

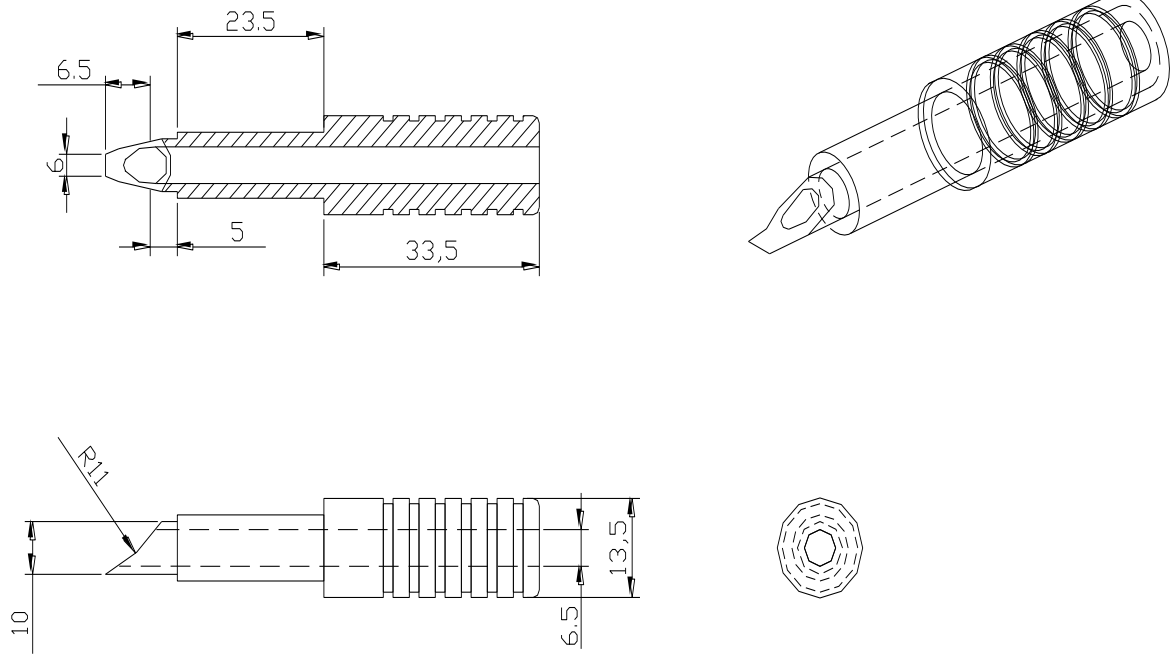


Fig. (5) Nozzle

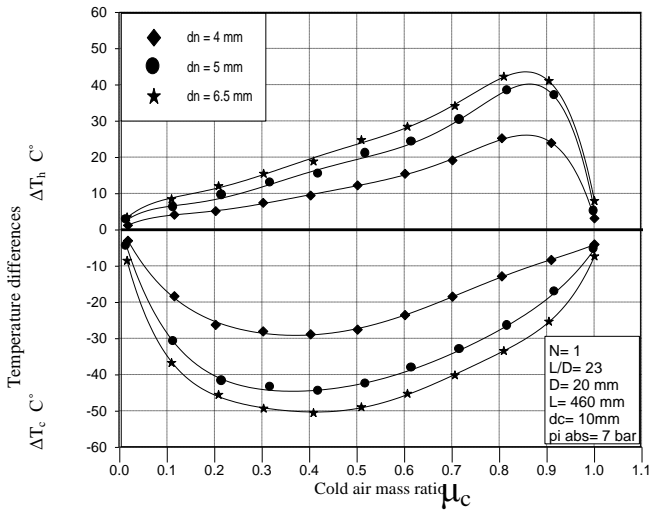


Fig. (6) Variation of temp. differences  $\Delta T_c$  &  $\Delta T_h$  with the mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^{\circ}=1.72$ ), with outlet diameter ( $d_n$ ) of the vortex tube as a parameter.

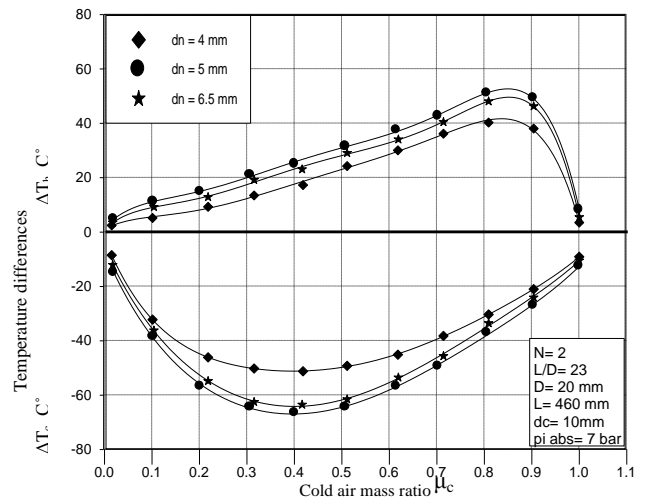


Fig. (7) Variation of temp. differences  $\Delta T_c$  &  $\Delta T_h$  with the cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^{\circ}=1.72$ ), with outlet nozzle diameter ( $d_n$ ) of the vortex tube as a parameter.

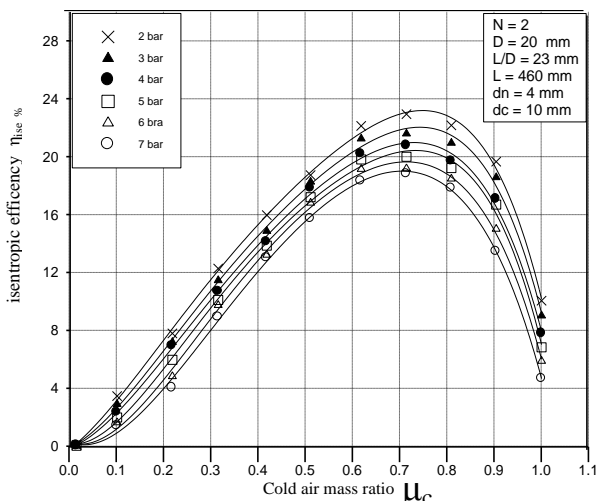


Fig. (8) The relation between isentropic efficiency ( $\eta_{ise}$ ) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^{\circ}=1.72$ ), with the absolute pressure ( $p_i$ ) of the inlet air as parameter.

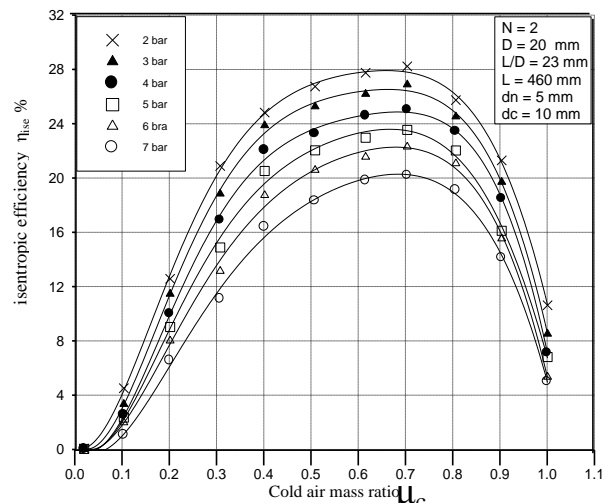


Fig. (9) The relation between isentropic efficiency ( $\eta_{ise}$ ) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^{\circ}=1.72$ ), with the absolute pressure ( $p_i$ ) of the inlet air as parameter.

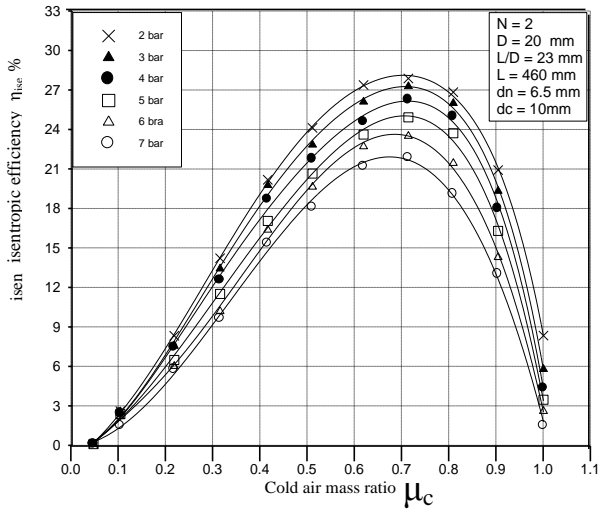


Fig. (10) The relation between isentropic efficiency ( $\eta_{ise}$ ) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^\circ = 1.72$ ), with the absolute pressure ( $p_1$ ) of the inlet air as parameter.

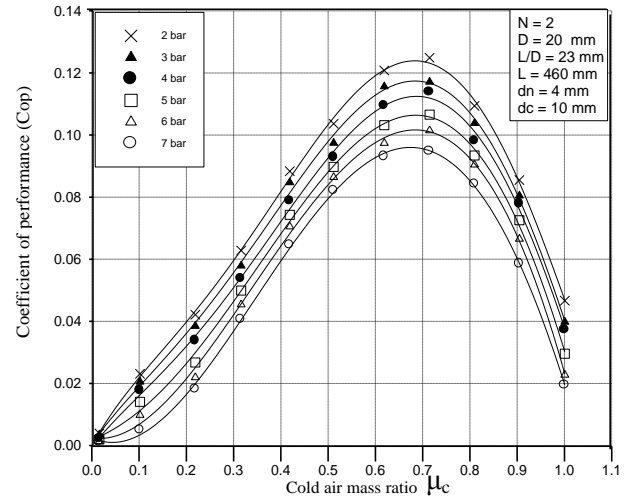


Fig. (11) The relation between coefficient of performance (Cop) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^\circ = 1.72$ ), with the absolute pressure ( $p_1$ ) of the inlet air as a parameter.

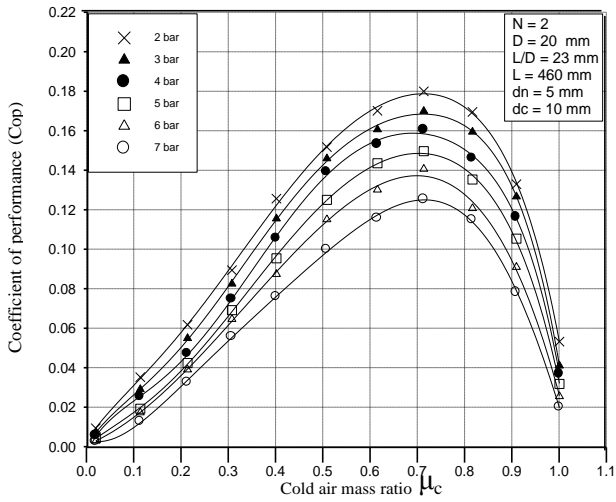


Fig. (12) The relation between coefficient of performance (Cop) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^\circ = 1.72$ ), with the absolute pressure ( $p_1$ ) of the inlet air as a parameter.

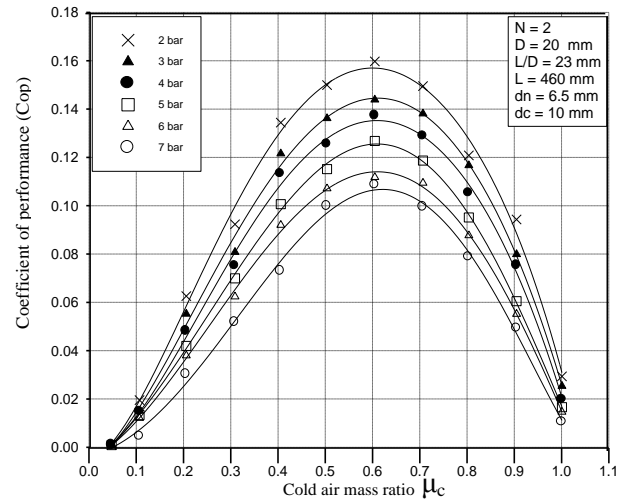


Fig. (13) The relation between coefficient of performance (Cop) and cold air mass ratio ( $\mu_c$ ) for vortex tube No.2 ( $\theta^\circ = 1.72$ ), with the absolute pressure ( $p_1$ ) of the inlet air as a parameter.

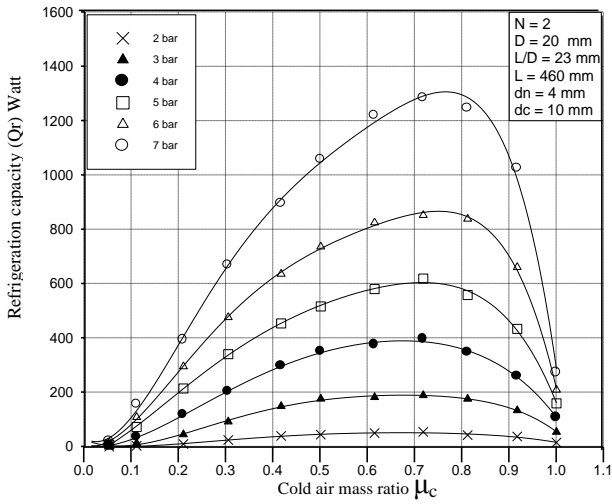


Fig. (14) The relation between Refrigeration capacity ( $Q_r$ ) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^\circ = 1.72$ ), with the absolute pressure ( $p_i$ ) of the inlet air as a parameter.

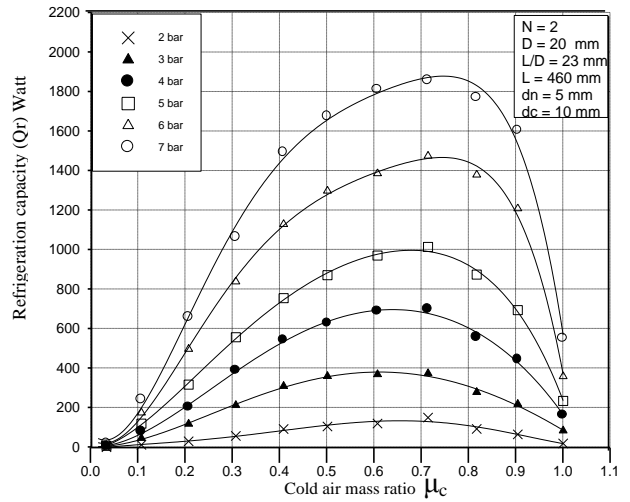


Fig. (15) The relation between Refrigeration capacity ( $Q_r$ ) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^\circ = 1.72$ ), with the absolute pressure ( $p_i$ ) of the inlet air as a parameter.

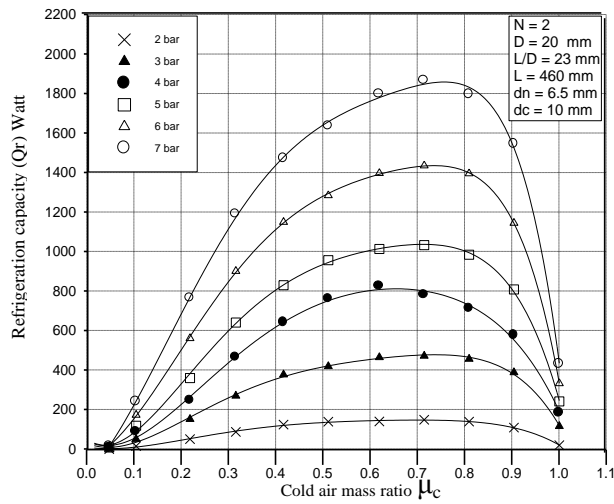


Fig. (16) The relation between Refrigeration capacity ( $Q_r$ ) and cold air mass ratio ( $\mu_c$ ) for vortex tube ( $\theta^\circ = 1.72$ ), with the absolute pressure ( $p_i$ ) of the inlet air as a parameter.